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Appendix A: Derivation of energy conservation equation as scalar variable temperature

1 ENERGY EQUATION FOR PURE AND ALLOY SYSTEM WITHOUT INTEGRATING FREE SURFACE

The energy conservation equation is derived on the basis of volume averaged continuum formulation originally proposed by [Benetton and Incropera, 1987a], as shown in below Eqn. 1.

$$\frac{\partial}{\partial t} \left(\sum_k g_k \rho_k h_k \right) + \nabla \cdot \left(\sum_k g_k \rho_k \vec{V}_k h_k \right) = \nabla \cdot (k \nabla T) \quad (1)$$

Mass averaged enthalpy is defined as $h = f_l h_l + f_s h_s$, where h_s and h_l are the respective phase enthalpies in solid and liquid defined as $h_s = c_{ps} T$ and $h_l = (c_{ps} - c_{pl}) T_S + h_{sl} + c_{pl} T$, respectively.

Expanding first term on left hand side of Eqn. 1 we get,

$$\frac{\partial}{\partial t} \left(\sum_k g_k \rho_k h_k \right) = \frac{\partial}{\partial t} (g_l \rho_l h_l + g_s \rho_s h_s) = \frac{\partial}{\partial t} (g_l \rho_l c_{pl} T + g_l \rho_l h_{sl} + g_l \rho_l c_{ps} T_S + g_s \rho_s c_{ps} T) \quad (2)$$

manipulating and arranging the above time derivative terms by adding and subtracting $g_l \rho_l c_{ps} T$ we get,

$$\begin{aligned} \frac{\partial}{\partial t} \left(\sum_k g_k \rho_k h_k \right) = \frac{\partial}{\partial t} (g_s \rho_s c_{ps} T + g_l \rho_l c_{ps} T + g_l \rho_l h_{sl} + g_l \rho_l c_{pl} T - g_l \rho_l c_{ps} T \\ - g_l \rho_l c_{pl} T_S + g_l \rho_l c_{ps} T_S) \end{aligned} \quad (3)$$

$$\frac{\partial}{\partial t} \left(\sum_k g_k \rho_k h_k \right) = \frac{\partial}{\partial t} (\rho c_{ps} T) + \frac{\partial}{\partial t} (g_l \rho_l h_{sl}) + \frac{\partial}{\partial t} (g_l \rho_l (c_{pl} - c_{ps})(T - T_S)) \quad (4)$$

Expanding second term on left hand side of Eqn. 1 we get,

$$\nabla \cdot \left(\sum_k g_k \rho_k \vec{V}_k h_k \right) = \nabla \cdot (g_l \rho_l \vec{V}_l h_l + g_s \rho_s \vec{V}_s h_s) \quad (5)$$

As velocity in solid domain is assumed to be zero, the term $g_s \rho_s \vec{V}_s h_s$ is zero and thus $g_l \rho_l \vec{V}_l = \rho \vec{V}$. Therefore equation becomes,

$$\begin{aligned} \nabla \cdot \left(\sum_k g_k \rho_k \vec{V}_k h_k \right) = \nabla \cdot (\rho \vec{V} c_{pl} T + \rho \vec{V} h_{sl} + \rho \vec{V} c_{ps} T_S - \rho \vec{V} c_{pl} T_S) = \nabla \cdot (\rho \vec{V} c_{pl} T) \\ + (h_{sl} + c_{ps} T_S - c_{pl} T_S) \nabla \cdot (\rho \vec{V}) \end{aligned} \quad (6)$$

$$\nabla \cdot \left(\sum_k g_k \rho_k \vec{V}_k h_k \right) = \nabla \cdot (\rho \vec{V} c_{pl} T) - (h_{sl} + c_{ps} T_S - c_{pl} T_S) \frac{\partial \rho}{\partial t} \quad (7)$$

substituting the above expression in Eqn. 1 we get,

$$\frac{\partial}{\partial t} (\rho c_{ps} T) + \nabla \cdot (\rho \vec{V} c_{pl} T) = \nabla \cdot (k \nabla T) - S \quad (8)$$

where s is the source term and is given as follows

$$S = \frac{\partial}{\partial t}(g_l \rho_l h_{sl}) + \frac{\partial}{\partial t}(g_l \rho_l (c_{pl} - c_{ps})(T - T_S)) - (h_{sl} + c_{ps} T_S - c_{pl} T_S) \frac{\partial \rho}{\partial t} \\ = \frac{\partial}{\partial t}(g_l \rho_l h_{sl} + g_l \rho_l (c_{pl} - c_{ps})(T - T_S) - (g_l \rho_l + (1 - g_l) \rho_s)(h_{sl} + c_{ps} T_S - c_{pl} T_S)) \quad (9)$$

Simplifying the above expression we get,

$$S = \frac{\partial}{\partial t}((g_l - 1) \rho_s h_{sl}) + \frac{\partial}{\partial t}(g_l \rho_l (c_{pl} - c_{ps}) T + (1 - g_l) \rho_s (c_{pl} - c_{ps}) T_S) \quad (10)$$

$$S = \frac{\partial}{\partial t}(g_l \rho_s h_{sl}) + \frac{\partial}{\partial t}(g_l (c_{pl} - c_{ps})(\rho_l T - \rho_s T_S)) \quad (11)$$

Therefore energy equation is,

$$\frac{\partial}{\partial t}(\rho c_{ps} T) + \nabla \cdot (\rho \vec{V} c_{pl} T) = \nabla \cdot (k \nabla T) - \frac{\partial}{\partial t}(g_l \rho_s h_{sl}) - \frac{\partial}{\partial t}(g_l (c_{pl} - c_{ps})(\rho_l T - \rho_s T_S)) \quad (12)$$

Further simplifying the equation in line with requirement we get,

$$\frac{\partial}{\partial t}(\rho T) + \nabla \cdot (\rho \vec{V} T) = \nabla \cdot \left(\frac{k}{c_{ps}} \nabla T \right) - \nabla \cdot \left[\left(\frac{c_{pl}}{c_{ps}} - 1 \right) \rho \vec{V} T \right] - \frac{\partial}{\partial t}(g_l \rho_s h_{sl}) \\ - \frac{\partial}{\partial t} \left[g_l \left(\frac{c_{pl}}{c_{ps}} - 1 \right) (\rho_l T - \rho_s T_S) \right] \quad (13)$$

2 ENERGY EQUATION FOR PURE AND ALLOY SYSTEM IN PRESENCE OF FREE SURFACE

Rewriting the Eqn. 9 we get,

$$S = \frac{\partial}{\partial t}(g_l \rho_l h_{sl}) + \frac{\partial}{\partial t}(g_l \rho_l (c_{pl} - c_{ps})(T - T_S)) - (h_{sl} + c_{ps} T_S - c_{pl} T_S) \frac{\partial \rho}{\partial t} \\ = \frac{\partial}{\partial t}(g_l \rho_l h_{sl} + g_l \rho_l (c_{pl} - c_{ps})(T - T_S) - (g_l \rho_l + g_s \rho_s)(h_{sl} + c_{ps} T_S - c_{pl} T_S)) \\ = \frac{\partial}{\partial t}(g_l \rho_l h_{sl} + g_l \rho_l (c_{pl} - c_{ps})(T - T_S) - (g_l \rho_l + (1 - g_l - g_v) \rho_s)(h_{sl} + c_{ps} T_S - c_{pl} T_S)) \quad (14)$$

Simplifying the above expression we get,

$$S = \frac{\partial}{\partial t}((g_l + g_v - 1) \rho_s h_{sl}) + \frac{\partial}{\partial t}(g_l \rho_l (c_{pl} - c_{ps}) T + (1 - g_l - g_v) \rho_s (c_{pl} - c_{ps}) T_S) \quad (15)$$

$$S = \frac{\partial}{\partial t}(g_l \rho_s h_{sl}) + \frac{\partial}{\partial t}(g_l (c_{pl} - c_{ps})(\rho_l T - \rho_s T_S)) + \frac{\partial}{\partial t}(g_v \rho_s h_{sl}) - \frac{\partial}{\partial t}(g_v \rho_s (c_{pl} - c_{ps}) T_S) \quad (16)$$

Further simplifying the equation in line with requirement we get,

$$\frac{\partial}{\partial t}(\rho c_{ps} T) + \nabla \cdot (\rho \vec{V} c_{pl} T) = \nabla \cdot (k \nabla T) - \frac{\partial}{\partial t}(g_l \rho_s h_{sl}) - \frac{\partial}{\partial t}(g_l (c_{pl} - c_{ps})(\rho_l T - \rho_s T_S)) - (\rho_s h_{sl} - \rho_s (c_{pl} - c_{ps}) T_S) \frac{\partial g_v}{\partial t} \quad (17)$$

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Appendix B: SIMPLER algorithm for solution of continuity and momentum equations

The fluid flow calculations performed for all the numerical models presented are obtained by solving continuity and momentum equations using Semi-Implicit Method for Pressure-Linked Equations Revised (SIMPLER) [Patankar, 2018]. A staggered grid arrangement is followed to solve the velocity field as shown in figure B1. The staggered grid arrangement eliminates the difficulties arising by estimating all the variables for the same grid nodes. The velocity flow field is obtained by solving momentum equations whereas the continuity equation is used to define the pressure field. To improve the convergence rate of the iterative method, a revised version has been worked out.

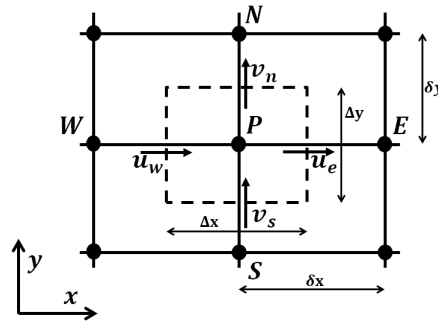


Figure B1 : Control volume for two-dimensional calculations.

A detailed mathematical formulation is given in [Patankar, 2018] and implies following sequence of operations:

1. Initially a flow field is assumed for an entire numerical domain.
2. The momentum equation in its simple form is written as,

$$u_e = \hat{u}_e + d_e(p_P - p_E) \quad (1)$$

where \hat{u}_e and d_e are defined as $\hat{u}_e = (\sum a_{nb}u_{nb} + b)/a_e$ and $d_e = A_e/a_e$ respectively. The term A_e is the area on which pressure difference acts; a_e is the coefficient of the discretised velocity equation; and b is the source term computed at velocity node e .

Calculate coefficients of these momentum equations to obtain \hat{u} and \hat{v} by substituting values of guessed flow field.

3. Once the velocity equation (from step 2) at all the faces are substituted into the discretised continuity equation, a pressure equation is obtained.

$$a_P p_P = \sum a_{nb} p_{nb} + b \quad (2)$$

where b in Eqn. 2 is given as

$$b = \frac{(\rho_P^0 - \rho_P)\Delta x \Delta y}{\Delta t} + [(\rho \hat{u})_w - (\rho \hat{u})_e]\Delta y + [(\rho \hat{v})_s - (\rho \hat{v})_n]\Delta x \quad (3)$$

Evaluate the values of the coefficients of the pressure equation Eqn. 1; $a_E = \rho_e d_e \Delta y$, $a_W = \rho_w d_w \Delta y$, $a_N = \rho_n d_n \Delta x$, and $a_S = \rho_s d_s \Delta x$. Eqn. 2 is then solved to obtain the pressure field.

4. The obtained pressure field is then treated as guess pressure field p^* to solve the discretised momentum equations,

$$a_e u_e^* = \sum a_{nb} u_{nb}^* + b + (p_P^* - p_E^*) A_e \quad (4)$$

$$a_n v_n^* = \sum a_{nb} v_{nb}^* + b + (p_P^* - p_N^*) A_n \quad (5)$$

Solving the equations we get u^* and v^*

5. Using u^* and v^* , the pressure correction equation is solved to obtain the values for p' .

$$a_P p'_P = \sum a_{nb} p'_{nb} + b \quad (6)$$

where coefficients a_P and a_{nb} are the same evaluated for pressure equation; and b is defined as

$$b = \frac{(\rho_P^0 - \rho_P) \Delta x \Delta y}{\Delta t} + [(\rho u^*)_w - (\rho u^*)_e] \Delta y + [(\rho v^*)_s - (\rho v^*)_n] \Delta x \quad (7)$$

6. Using velocity correction formula as given

$$u_e = u_e^* + d_e (p'_P - p'_E) \quad (8)$$

$$v_n = v_n^* + d_n (p'_P - p'_N) \quad (9)$$

correct the flow field, but pressure correction is unnecessary.

7. Once flow field is obtained, solve discretised equations for other scalar quantities viz., temperature T and concentration C , respectively.
8. Repeat the procedure from step 2 until desired convergence is obtained.

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Appendix C: Volume of Fluid Method

For the present investigation a volume of fluid (VOF) method is implemented to track the interface motion between solidifying melt and void section. The method is implemented to obtain the void fraction g_v , by solving the advection equation (Eqn. 1). Since the flow field conserves the shape and void fraction volume, g_v satisfies the advection equation,

$$\frac{\partial}{\partial t}(g_v) + \nabla \cdot (g_v \mathbf{V}) = g_v (\nabla \cdot \mathbf{V}) \quad (1)$$

Further to solve the eqn. 1, the operator splitting method is employed that results into two different equations varying in x and y direction independently [Gerlach et al., 2006; Puckett et al., 1997].

$$\frac{\partial}{\partial t}(g_v) + \frac{\partial}{\partial x}(g_v u) = g_v \frac{\partial u}{\partial x} \quad (2)$$

$$\frac{\partial}{\partial t}(g_v) + \frac{\partial}{\partial y}(g_v v) = g_v \frac{\partial v}{\partial y} \quad (3)$$

In order to sustain the conservation of void fraction g_v it is required to discretise implicitly on right hand side of eqn. 2 and explicitly on right hand side of eqn. 3. Use of implicit-explicit scheme in alternate sweep directions assists in obtaining the second order accuracy. The final discretised equations are given below with reference to figure C1(a),

$$(g'_v)_{i,j} = \left[(g_v^n)_{i,j} + \frac{1}{\Delta x} (\delta F_{i-1/2,j} - \delta F_{i+1/2,j}) \right] / \left[1 - \frac{\Delta t}{\Delta x} (u_{i-1/2,j} - u_{i+1/2,j}) \right] \quad (4)$$

$$(g_v^{n+1})_{i,j} = (g'_v)_{i,j} \left[1 + \frac{\Delta t}{\Delta y} (v_{i,j+1/2} - v_{i,j-1/2}) \right] + \frac{1}{\Delta y} (\delta F'_{i,j-1/2} - \delta F'_{i,j+1/2}) \quad (5)$$

where δF is the amount of liquid void fraction that is fluxed through the cell face. The superscript (') used in eqn. 5 simply denotes the void flux value at intermediate stage after the first sweep in x-direction.

The important operation is now to calculate the δF for the above discretised eqns. 4 and 5 in such a manner that the conservation of void fraction is followed and no numerical augmentation is instigated. This is performed by following the donor-acceptor scheme proposed by Hirt and Nichols [1981]. Figure C1(b) considers the fluid flow configuration with a positive fluid flow in x-direction at face $i + \frac{1}{2}$. The donor-acceptor method estimates the volume flux across node $(i + \frac{1}{2}, j)$ as,

$$\delta F_{i+1/2,j} = \Delta y \left\{ \text{MIN} \left[(g_v)_{i,j} \delta x, u_{i+1/2,j} (g_v)_{i+1,j} \delta t + \text{MAX} \left(0.0, u_{i+1/2,j} (1 - (g_v)_{i+1,j}) \delta t - (1 - (g_v)_{i,j}) \delta x \right) \right] \right\} \quad (6)$$

The MIN feature in eqn. 6 prevents the additional fluxing of fluid from cell (i, j) through face $(i + \frac{1}{2}, j)$ whereas the max feature ensures that no more void volume is fluxed out of cell (i, j) .

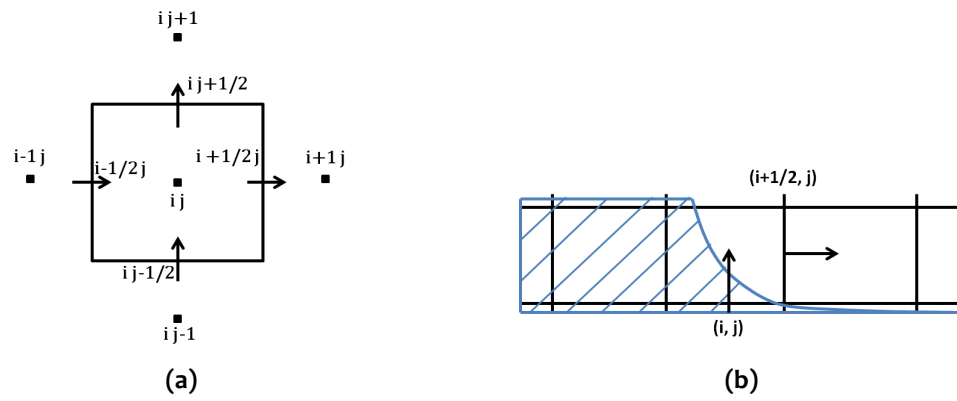


Figure C1: (a) Discretised representation of control volume and (b) Interface configuration for Hirt-Nichols VOF model.

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Appendix D: List of publications from the present investigation

D1 JOURNAL ARTICLES

1. Monde AD, Shrivastava A, Jakhar A, Chakraborty PR. "Binary alloy solidification and freckle formation: Effect of shrinkage induced flow on solutal instability and macro-segregation" *Physics of Fluids*. 2021 Mar 1;33(3):037108.
2. Monde AD, Chawla O, Kumar V, Karagadde S, Chakraborty PR. "Shrinkage induced flow during directional solidification of pure substance in a bottom cooled cavity: A study on flow reversal phenomena" *Physics of Fluids* 2020 Apr 1;32(4):047104.
3. Monde AD, Chakraborty PR. "Prediction of cooling curves for controlled unidirectional solidification under the influence of shrinkage: a semi-analytical approach" *Metallurgical and Materials Transactions B*. 2018 Dec 1;49(6):3306-16.
4. Monde AD, Chakraborty PR. "1-D diffusion based solidification model with volumetric expansion and shrinkage effect: A semi-analytical approach" *Physics Letters A*. 2017 Oct 17;381(39):3349-54.

D2 CONFERENCES

1. Monde AD, Jakhar A, Chakraborty PR. "Effect of shrinkage during thermo-solutal convection for a unidirectional solidification of binary alloys" *8th International and 47th National Conference on Fluid Mechanics and Fluid Power (FMFP-2020)* 2020
2. Monde AD, Chawla O, Chakraborty PR. "Numerical Analysis of Shrinkage Induced Convection during Bottom up Solidification of Pure Material" *25th National and 3rd International ISHMT-ASTFE Heat and Mass Transfer Conference (IHMTTC-2019)* 2019
3. Monde AD, Bhattacharya A, Chakraborty PR. "Shrinkage induced flow and Free surface evolution during solidification of pure metal" *In E3S Web of Conferences 2019 (Vol. 128, p. 06011)*. EDP Sciences.
4. Kumar C, Monde AD, Bhattacharya A, Chakraborty PR. "Modeling of dendrite growth in undercooled solution sodium acetate trihydrate" *In E3S Web of Conferences 2019 (Vol. 128, p. 01023)*. EDP Sciences.
5. Monde AD, Chawla O, Bhuyar V, Vijay M, Chakraborty PR. "Performance evaluation of latent heat based cool pack configuration for thermal comfort: A numerical approach" *International Conference on Computational Methods for Thermal Problems 2018*